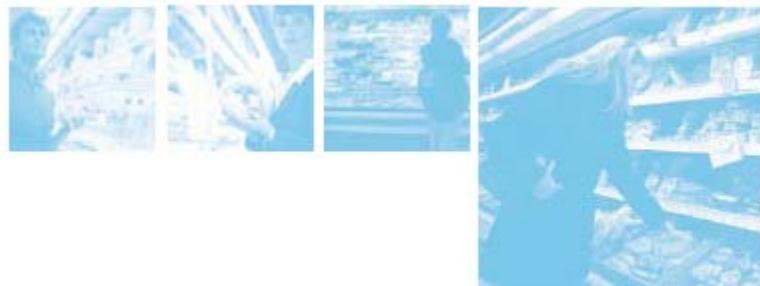


KLEEA® 407C

Engineers' Tables SI Units



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FLUOR

1. Introduction

The following tables provide practical information to help you design or set up refrigeration systems using KLEA®407C. We've tried to make the layout as easy as possible to use; where possible we've followed the existing conventions used in standard reference works. These tables are supplementary to the Physical Property Datasheet for KLEA®407C and the booklets of Thermodynamic Property Data for KLEA®407C.

2. Temperature-Pressure Tables for KLEA®407C

2.1 Evaporator and Condenser Tables

The temperature glide need cause no problems so long as you know the correct relationship between pressure and temperature for the evaporator and the condenser. If you are unsure about the basic behaviour of blended refrigerants, refer to the Mexichem Fluor Technical Note Introduction to Mixed Refrigerants for further guidance. Bear in mind:

- When specifying the evaporating and condensing temperatures we set mean temperatures in these exchangers.
- When setting evaporator superheat we calculate it from the saturated vapour or dew point temperature in the evaporator.
- When setting subcool we calculate it from the saturated liquid or bubble point temperature in the condenser.

The following simple guidelines explain which tables to use to obtain the relationships between the saturated liquid and vapour pressures and temperatures. We have tabulated the following data for you:

Table 1: Evaporator pressure from condenser liquid temperature and evaporator mean temperature.

Table 2: Evaporator temperature from condenser liquid temperature and evaporator pressure.

Table 3: Evaporator saturated vapour temperature from pressure (dew point).

Table 4: Condenser pressure from mean temperature.

Table 5-7: Maximum recommended suction line capacities for varying suction gas conditions.

Table 8: Discharge line capacities.

Table 9: Liquid line capacities.

Table 10: Recommended minimum capacities for oil entrainment in suction lines.

Table 11: Correction factors for use with the capacity tables at other conditions.

Refrigerant Flowrate: A graphical correlation of refrigerant flowrate per unit capacity.

2.2 Using the Tables

- In setting up a system to give a specified mean evaporating temperature, you simply look up the pressure you need in the evaporator using the temperature of liquid at the expansion valve and the mean temperature you want in Table 1.
- The liquid temperature at the valve has only a slight effect on the mean temperature but we have tabulated it nonetheless. For practical purposes the evaporator pressure will not vary significantly even if the liquid temperature at the valve changes.
- To set the mean temperature for the condenser just look up the mean condensing pressure in Table 4.
- To calculate the superheat for a given pressure, use the table of saturated vapour temperatures (dew points) to give you the saturation temperature for the vapour leaving the evaporator.
- To calculate the subcooling for a given pressure, use the table of saturated liquid temperature (bubble point) as a function of pressure.
- You can also readily estimate the mean temperatures from pressure readings using these tables.
- The capacity tables follow the standard layouts used in other reference sources.

2.3 Worked examples for mean pressure/temperature tables:

(i) Setting the evaporator pressure

Problem:

Liquid temperature at valve: 40 °C.

Desired evaporating temperature: -15 °C.

What is the evaporator pressure to use?

What is the effect of a liquid temperature of 30 °C?

Solution:

For KLEA®407C, with a liquid temperature at the valve of 40 °C and a desired mean evaporating temperature of -15 °C, read Table 1 to get an evaporator pressure of 2.87 bara. A liquid temperature of 30 °C gives an evaporator pressure of 2.89 bara...a change of 1%.

(ii) Finding the evaporator temperature from a gauge reading:

Problem:

Evaporator pressure gauge reads 2.5 bara.

Measured exit temperature (from thermometer) is -15.5 °C.

What is the mean evaporator temperature?

What is the superheat in the evaporator?

Solution:

For KLEA®407C, we have a measured evaporator pressure of 2.5 bara and a measured exit temperature of -12.5 °C; we want to check superheat and evaporating temperature. The liquid temperature is 40 °C. Table 2 shows that the mean evaporating temperature is -18.4 °C. The superheat is calculated from the dewpoint, which is -16.4 °C; hence we have a working superheat of 3.9 °C, obtained by subtracting the dew point temperature from the measured exit temperature.

(iii) Setting up the condenser pressure and subcool.

Problem:

Target mean condenser temperature is 40 °C.

The liquid temperature at the valve will be 30 °C.

What is the condensing pressure?

What degree of subcooling will be required?

Solution:

Table 3 supplies the condenser pressure of 16.5 bara for a mean condenser of 40 °C. Then the subcooling is obtained by subtracting the liquid temperature of 30 °C from the bubble point of 37.4 °C, giving a subcool of 7.4°C.

3. Refrigerant Line Capacity Tables

3.1 Methods used to generate the tables

The tables presented here have been developed using the methodology described in the ASHRAE Handbook: Refrigeration Systems and Applications (1994). The physical property data used to generate these tables are correlated in the Mexichem Fluor datasheets, thermodynamic tables. Pressure drop has been estimated using the Colebrook equation to obtain friction factors and the Darcy-Weisbach equation for pressure drop.

Gas Compressibility Effects

In calculating the maximum capacity (flowrate) it has been assumed that the gas is incompressible. This is in line with the tables published in the ASHRAE Handbook and for most systems this is perfectly adequate.

The assumption of incompressibility may however over-predict capacity if the total pressure drop is appreciable compared to the static pressure. The likely over-prediction will be in the region of 5-10% depending on the evaporator pressure and total line loss (including fittings loss).

Mexichem Fluor recommends that the pressure drop obtained for a line using these tables should be compared to the total pressure available; if it is greater than 5% of the static pressure then the compressibility may have some effect, and sizing should be made on that basis.

3.2 Suction Line Capacity Tables

These tables give capacities for cycles operating under the following conditions:

Condenser mean temperature 40 °C.

Zero subcooling (i.e. liquid at bubble point).

Vapour leaving evaporator (i) saturated i.e. at dew point or (ii) superheated (superheat quoted in the table).

Evaporator temperatures quoted are true mean values.

The capacity for other liquid temperatures may be found using the tabulated correction factors given in Table 11. Note that the tables are referenced to a mean condenser of 40 °C; the liquid temperature (bubble point) corresponding to this condition is quoted in the tables.

The tables quote capacity for pressure drops in the mean evaporating pressure equivalent to a drop in saturation temperature of 0.01, 0.02 and 0.04 Kelvin for every metre of suction line. Data are presented for copper tubing, Type L, and Schedule 40 steel pipe with dimensions as given in the ASHRAE Handbook HVAC Systems and Equipment (1992).

The mass flowrate of refrigerant is also presented graphically as the flow in kg/hr required for a duty of 1 kW refrigeration over a range of evaporating temperatures and liquid temperatures.

3.3 Discharge Line Capacity Tables

These have been calculated on the following basis:

Condenser mean temperature of 40 °C.
Zero subcooling i.e. liquid at bubble point.
Vapour leaves evaporator at dew point i.e. zero useful superheat.
Superheat at compressor discharge is (i) 45 or (ii) 60 °C.
Evaporator temperatures are true mean values.

3.4 Liquid Line Capacity Tables

These are quoted for conditions of (i) 0.5 m/s maximum velocity or (ii) 0.02 K/m drop in saturation temperature. Use the velocity criterion for sizing self-venting lines.

3.5 Correcting for other Temperature Drops or Line Lengths

The suction capacity tables reference according to saturation temperature losses of 0.01, 0.02 and 0.04 K in one metre length. In order to correct the capacities for different values of temperature drop or line length, use the following equation:

$$\text{Actual Capacity} = \text{Table Capacity} \times \left(\frac{\text{Required } \Delta T_e}{\text{Table } \Delta T_e} \times \frac{\text{Table } L_e}{\text{Required } L_e} \right)^{0.54}$$

where:

ΔT_e is the change in mean evaporating temperature at evaporator pressure

L_e is the length of suction line

To evaluate the change in saturation temperature for differing capacities or line lengths, use the equation:

$$\text{Actual } \Delta T_e = \text{Table } \Delta T_e \times \left(\frac{\text{Actual } L_e}{\text{Table } L_e} \right) \times \left[\frac{\text{Actual Capacity}}{\text{Table Capacity}} \right]^{1.8}$$

4. What's New In This Edition

This is version 1.1 of the Tables. The updates from version 1.0 are as follows:

- **Tables 5-9:** A revision of the physical property routines and calculation methods has occurred so that all physical properties used in the calculation are now obtained from the most recent physical property datasheets for each refrigerant.
- **Tables 5-9:** The nomenclature in the tables has been changed slightly to make it more readable.
- **Tables 5-11:** The number of significant figures in the tables is revised to three to better reflect the accuracy limits of the calculations.
- **Table 10:** The oil-refrigerant calculations have been carried out using new data for the solubility of KLEA®407A in UNIQEMA EMKARATEM RL 32S and RL68S lubricants.
- **Table 11:** The changes in physical property calculations have resulted in some changes to the correction factors displayed in this table.

Table I: Evaporator pressure from liquid temperature and mean evaporating temperature

KLEA 407C

Pressure in bara

Temp. mean °C	Temperature liquid °C		
	30	40	50
5	5.94	5.89	5.84
4	5.75	5.70	5.65
3	5.56	5.51	5.46
2	5.37	5.33	5.28
1	5.19	5.15	5.10
0	5.02	4.98	4.93
-1	4.85	4.81	4.76
-2	4.68	4.64	4.60
-3	4.52	4.48	4.44
-4	4.36	4.32	4.28
-5	4.21	4.17	4.13
-6	4.06	4.02	3.99
-7	3.91	3.88	3.84
-8	3.77	3.74	3.70
-9	3.64	3.60	3.57
-10	3.50	3.47	3.44
-11	3.37	3.34	3.31
-12	3.25	3.22	3.19
-13	3.13	3.10	3.07
-14	3.01	2.98	2.95
-15	2.89	2.87	2.84
-16	2.78	2.76	2.73
-17	2.67	2.65	2.62
-18	2.57	2.54	2.52
-19	2.47	2.44	2.42
-20	2.37	2.35	2.32
-21	2.27	2.25	2.23
-22	2.18	2.16	2.14
-23	2.09	2.07	2.05
-24	2.00	1.98	1.96
-25	1.92	1.90	1.88
-26	1.84	1.82	1.80
-27	1.76	1.74	1.72
-28	1.68	1.67	1.65
-29	1.61	1.59	1.58
-30	1.54	1.52	1.51
-31	1.47	1.46	1.44
-32	1.41	1.39	1.38
-33	1.34	1.33	1.31
-34	1.28	1.27	1.25
-35	1.22	1.21	1.19
-36	1.17	1.15	1.14
-37	1.11	1.10	1.09
-38	1.06	1.05	1.03
-39	1.01	1.00	0.98
-40	0.96	0.95	0.94

Table 2: Mean evaporator temperature from pressure and liquid temperature

KLEA 407C

Pressure bara	Temperature liquid °C			Temp. dew °C
	30	40	50	
1	-39.16	-38.92	-38.67	-37.10
1.1	-37.21	-36.98	-36.72	-35.14
1.2	-35.40	-35.16	-34.91	-33.31
1.3	-33.70	-33.47	-33.21	-31.60
1.4	-32.11	-31.87	-31.62	-29.99
1.5	-30.60	-30.36	-30.11	-28.46
1.6	-29.16	-28.93	-28.67	-27.01
1.7	-27.80	-27.56	-27.31	-25.63
1.8	-26.49	-26.26	-26.00	-24.32
1.9	-25.25	-25.01	-24.76	-23.06
2	-24.05	-23.81	-23.56	-21.84
2.1	-22.90	-22.66	-22.40	-20.68
2.2	-21.79	-21.55	-21.29	-19.56
2.3	-20.71	-20.48	-20.22	-18.47
2.4	-19.68	-19.44	-19.18	-17.42
2.5	-18.67	-18.43	-18.18	-16.41
2.6	-17.70	-17.46	-17.20	-15.42
2.7	-16.75	-16.52	-16.26	-14.47
2.8	-15.84	-15.60	-15.34	-13.54
2.9	-14.94	-14.70	-14.44	-12.63
3	-14.07	-13.83	-13.57	-11.75
3.1	-13.22	-12.98	-12.73	-10.89
3.2	-12.40	-12.16	-11.90	-10.06
3.3	-11.59	-11.35	-11.09	-9.24
3.4	-10.80	-10.56	-10.30	-8.44
3.5	-10.03	-9.79	-9.53	-7.66
3.6	-9.27	-9.03	-8.77	-6.90
3.7	-8.54	-8.29	-8.03	-6.15
3.8	-7.81	-7.57	-7.31	-5.42
3.9	-7.10	-6.86	-6.60	-4.70
4	-6.41	-6.17	-5.90	-4.00
4.1	-5.73	-5.48	-5.22	-3.31
4.2	-5.06	-4.81	-4.55	-2.63
4.3	-4.40	-4.16	-3.89	-1.97
4.4	-3.75	-3.51	-3.25	-1.31
4.5	-3.12	-2.88	-2.61	-0.67
4.6	-2.49	-2.25	-1.99	-0.04
4.7	-1.88	-1.64	-1.38	0.58
4.8	-1.28	-1.03	-0.77	1.19
4.9	-0.68	-0.44	-0.18	1.79
5	-0.10	0.15	0.41	2.38
5.1	0.48	0.72	0.98	2.96
5.2	1.05	1.29	1.55	3.54
5.3	1.60	1.85	2.11	4.10
5.4	2.16	2.40	2.66	4.66
5.5	2.70	2.94	3.21	5.21
5.6	3.23	3.48	3.74	5.75
5.7	3.76	4.01	4.27	6.28
5.8	4.29	4.53	4.79	6.81
5.9	4.80	5.04	5.31	7.33
6	5.31	5.55	5.82	7.84

Note: Superheat should be set from dew point

Pressure bara	Temperature liquid °C			Temp. dew °C
	30	40	50	
6.1	5.81	6.05	6.32	8.35
6.2	6.31	6.55	6.81	8.85
6.3	6.79	7.04	7.30	9.34
6.4	7.28	7.52	7.79	9.83
6.5	7.76	8.00	8.27	10.31
6.6	8.23	8.47	8.74	10.79
6.7	8.69	8.94	9.21	11.26
6.8	9.16	9.40	9.67	11.73
6.9	9.61	9.86	10.12	12.19
7	10.06	10.31	10.57	12.64
7.1	10.51	10.76	11.02	13.09
7.2	10.95	11.20	11.46	13.54
7.3	11.39	11.63	11.90	13.98
7.4	11.82	12.07	12.33	14.42
7.5	12.25	12.49	12.76	14.85
7.6	12.67	12.92	13.18	15.27
7.7	13.09	13.34	13.60	15.70
7.8	13.51	13.75	14.02	16.12
7.9	13.92	14.16	14.43	16.53
8	14.33	14.57	14.84	16.94
8.1	14.73	14.97	15.24	17.35
8.2	15.13	15.37	15.64	17.75
8.3	15.52	15.77	16.04	18.15
8.4	15.92	16.16	16.43	18.54
8.5	16.31	16.55	16.82	18.94
8.6	16.69	16.94	17.20	19.32
8.7	17.07	17.32	17.58	19.71
8.8	17.45	17.70	17.96	20.09
8.9	17.83	18.07	18.34	20.47
9	18.20	18.44	18.71	20.84
9.1	18.57	18.81	19.08	21.21
9.2	18.93	19.18	19.44	21.58
9.3	19.30	19.54	19.81	21.95
9.4	19.65	19.90	20.17	22.31
9.5	20.01	20.26	20.52	22.67
9.6	20.37	20.61	20.88	23.02
9.7	20.72	20.96	21.23	23.38
9.8	21.07	21.31	21.58	23.73
9.9	21.41	21.66	21.92	24.08
10	21.75	22.00	22.27	24.42

Note: Superheat should be set from dew point

Table 3: Condenser mean pressure, dew and bubble points, from the mean temperature

KLEA 407C

Mean temp. °C	Pressure bara	Bubble/liquid temp. °C	Dew temp. °C
10	7.10	6.89	13.10
11	7.32	7.91	14.08
12	7.55	8.92	15.07
13	7.79	9.93	16.06
14	8.03	10.95	17.04
15	8.27	11.96	18.03
16	8.52	12.98	19.01
17	8.78	13.99	20.00
18	9.04	15.01	20.99
19	9.31	16.02	21.97
20	9.58	17.04	22.95
21	9.86	18.06	23.94
22	10.15	19.07	24.92
23	10.44	20.09	25.90
24	10.74	21.11	26.89
25	11.04	22.13	27.87
26	11.35	23.14	28.85
27	11.67	24.16	29.83
28	12.00	25.18	30.81
29	12.33	26.20	31.79
30	12.67	27.22	32.77
31	13.01	28.24	33.75
32	13.37	29.26	34.73
33	13.73	30.28	35.71
34	14.09	31.30	36.69
35	14.47	32.32	37.67
36	14.85	33.34	38.65
37	15.24	34.36	39.63
38	15.64	35.38	40.60
39	16.05	36.41	41.58
40	16.46	37.43	42.56
41	16.88	38.45	43.53
42	17.31	39.47	44.51
43	17.75	40.50	45.49
44	18.20	41.52	46.46
45	18.65	42.55	47.44
46	19.12	43.57	48.41
47	19.59	44.60	49.38
48	20.07	45.62	50.36
49	20.56	46.65	51.33
50	21.06	47.67	52.31
51	21.57	48.70	53.28
52	22.09	49.73	54.25
53	22.62	50.75	55.22
54	23.16	51.78	56.20
55	23.70	52.81	57.17
56	24.26	53.84	58.14
57	24.83	54.87	59.11
58	25.41	55.90	60.08
59	25.99	56.92	61.05
60	26.59	57.96	62.03

Note: Subcool is measured from bubble point

Table 4: Condenser bubble, dew and mean temperatures from condenser pressure

KLEA 407C

Pressure bara	Temperatures °C		
	Bubble/liquid	Mean	Dew
10	18.56	21.49	24.42
10.2	19.26	22.18	25.10
10.4	19.96	22.87	25.78
10.6	20.64	23.54	26.44
10.8	21.32	24.21	27.09
11	21.99	24.86	27.73
11.2	22.64	25.51	28.37
11.4	23.29	26.14	28.99
11.6	23.93	26.77	29.61
11.8	24.57	27.39	30.22
12	25.19	28.01	30.82
12.2	25.81	28.61	31.42
12.4	26.42	29.21	32.00
12.6	27.02	29.80	32.58
12.8	27.61	30.38	33.15
13	28.20	30.96	33.72
13.2	28.78	31.53	34.27
13.4	29.35	32.09	34.83
13.6	29.92	32.65	35.37
13.8	30.48	33.20	35.91
14	31.04	33.74	36.44
14.2	31.59	34.28	36.97
14.4	32.13	34.81	37.49
14.6	32.67	35.34	38.01
14.8	33.20	35.86	38.52
15	33.73	36.38	39.02
15.2	34.25	36.89	39.52
15.4	34.77	37.39	40.02
15.6	35.28	37.90	40.51
15.8	35.79	38.39	40.99
16	36.29	38.88	41.47
16.2	36.79	39.37	41.95
16.4	37.28	39.85	42.42
16.6	37.77	40.33	42.89
16.8	38.26	40.80	43.35
17	38.74	41.27	43.81
17.2	39.21	41.74	44.26
17.4	39.68	42.20	44.71
17.6	40.15	42.65	45.15
17.8	40.61	43.11	45.60
18	41.07	43.55	46.03
18.2	41.53	44.00	46.47
18.4	41.98	44.44	46.90
18.6	42.43	44.88	47.33
18.8	42.88	45.31	47.75
19	43.32	45.74	48.17
19.2	43.75	46.17	48.58
19.4	44.19	46.59	49.00
19.6	44.62	47.01	49.41
19.8	45.05	47.43	49.81
20	45.47	47.84	50.22

Pressure bara	Temperatures °C		
	Bubble/liquid	Mean	Dew
20.2	45.89	48.26	50.62
20.4	46.31	48.66	51.01
20.6	46.73	49.07	51.41
20.8	47.14	49.47	51.80
21	47.55	49.87	52.19
21.2	47.95	50.26	52.57
21.4	48.36	50.66	52.95
21.6	48.76	51.05	53.33
21.8	49.16	51.43	53.71
22	49.55	51.82	54.09
22.2	49.94	52.20	54.46
22.4	50.33	52.58	54.83
22.6	50.72	52.96	55.19
22.8	51.10	53.33	55.56
23	51.49	53.70	55.92
23.2	51.86	54.07	56.28
23.4	52.24	54.44	56.63
23.6	52.62	54.80	56.99
23.8	52.99	55.16	57.34
24	53.36	55.52	57.69
24.2	53.73	55.88	58.04
24.4	54.09	56.24	58.38
24.6	54.45	56.59	58.72
24.8	54.82	56.94	59.06
25	55.17	57.29	59.40
25.2	55.53	57.63	59.74
25.4	55.88	57.98	60.07
25.6	56.24	58.32	60.41
25.8	56.59	58.66	60.74
26	56.93	59.00	61.06
26.2	57.28	59.34	61.39
26.4	57.62	59.67	61.71
26.6	57.97	60.00	62.04
26.8	58.31	60.33	62.36
27	58.65	60.66	62.68
27.2	58.98	60.99	62.99
27.4	59.32	61.31	63.31
27.6	59.65	61.63	63.62
27.8	59.98	61.96	63.93
28	60.31	62.28	64.24
28.2	60.64	62.59	64.55
28.4	60.96	62.91	64.86
28.6	61.29	63.22	65.16
28.8	61.61	63.54	65.46
29	61.93	63.85	65.76
29.2	62.25	64.16	66.06
29.4	62.56	64.46	66.36
29.6	62.88	64.77	66.66
29.8	63.19	65.07	66.95
30	63.51	65.38	67.25

Table 5a: Suction line capacities in kW for KLEA 407C
Saturated vapour leaving evaporator

Nominal line size mm	T $\Delta P/\Delta L$	Saturation temperature change 1.0 K in 100 m									
		Mean evaporating temperature °C at corresponding pressure drop, Pa/m									
		-40 48	-35 58	-30 70	-25 82	-20 97	-15 113	-10 130	-5 150	0 172	5 195
Type L Copper											
10		0.068	0.086	0.110	0.139	0.174	0.215	0.264	0.320	0.386	0.462
12		0.158	0.201	0.257	0.324	0.404	0.499	0.611	0.741	0.892	1.07
15		0.300	0.381	0.487	0.614	0.765	0.944	1.15	1.40	1.68	2.01
19		0.517	0.656	0.837	1.05	1.31	1.62	1.98	2.39	2.88	3.44
22		0.804	1.02	1.30	1.64	2.04	2.51	3.07	3.71	4.46	5.32
28		1.64	2.09	2.66	3.35	4.16	5.12	6.25	7.55	9.07	10.8
35		2.89	3.67	4.67	5.86	7.28	8.96	10.9	13.2	15.8	18.9
42		4.59	5.83	7.42	9.31	11.6	14.2	17.3	20.9	25.1	29.9
54		9.59	12.2	15.5	19.4	24.1	29.6	36.0	43.5	52.1	62.1
67		17.0	21.7	27.5	34.5	42.8	52.5	63.9	77.0	92.3	110
79		27.3	34.7	44.1	55.2	68.4	83.9	102	123	147	175
92		40.7	51.8	65.7	82.3	102	125	152	183	219	261
105		57.6	73.3	92.9	116	144	177	215	259	309	368
Schedule 40 steel											
10		0.204	0.259	0.327	0.408	0.503	0.614	0.742	0.890	1.06	1.25
15		0.380	0.484	0.611	0.761	0.937	1.14	1.38	1.66	1.97	2.33
20		0.808	1.03	1.29	1.61	1.98	2.41	2.92	3.49	4.15	4.91
25		1.54	1.95	2.46	3.06	3.76	4.58	5.53	6.62	7.87	9.30
32		3.19	4.05	5.09	6.33	7.77	9.46	11.4	13.7	16.2	19.2
40		4.80	6.10	7.66	9.51	11.7	14.2	17.1	20.5	24.4	28.8
50		9.30	11.8	14.8	18.4	22.6	27.5	33.1	39.6	47.0	55.5
65		14.9	18.9	23.7	29.4	36.1	43.8	52.8	63.2	75.0	88.6
80		26.4	33.5	42.0	52.0	63.8	77.5	93.4	112	133	157
100		53.9	68.3	85.7	106	130	158	190	228	270	319

Note: (i) Capacity based on saturated vapour (no useful superheat)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 5b: Suction line capacities in kW for KLEA 407C
Saturated vapour leaving evaporator

Nominal line size mm	T $\Delta P/\Delta L$	Saturation temperature change 2.0 K in 100 m									
		Mean evaporating temperature °C at corresponding pressure drop, Pa/m									
		-40 96	-35 116	-30 139	-25 165	-20 193	-15 225	-10 261	-5 300	0 343	5 391
Type L Copper											
10		0.101	0.128	0.164	0.207	0.258	0.319	0.390	0.473	0.569	0.680
12		0.234	0.297	0.380	0.479	0.597	0.736	0.899	1.09	1.31	1.56
15		0.443	0.564	0.719	0.905	1.13	1.39	1.70	2.05	2.47	2.94
19		0.760	0.968	1.23	1.55	1.93	2.38	2.90	3.51	4.21	5.02
22		1.18	1.50	1.91	2.41	2.99	3.68	4.49	5.43	6.52	7.77
28		2.41	3.07	3.91	4.91	6.10	7.49	9.13	11.0	13.2	15.8
35		4.23	5.38	6.84	8.58	10.7	13.1	15.9	19.2	23.1	27.5
42		6.71	8.55	10.9	13.6	16.9	20.7	25.2	30.5	36.5	43.4
54		14.0	17.8	22.6	28.4	35.1	43.1	52.4	63.2	75.7	90.0
67		24.9	31.7	40.1	50.3	62.3	76.3	92.8	112	134	159
79		39.8	50.7	64.2	80.4	99.5	122	148	178	213	254
92		59.3	75.5	95.6	120	148	181	220	265	317	377
105		83.8	107	135	169	209	256	311	374	447	531
Schedule 40 steel											
10		0.294	0.374	0.472	0.587	0.722	0.880	1.06	1.27	1.51	1.79
15		0.549	0.698	0.878	1.09	1.34	1.63	1.97	2.36	2.81	3.32
20		1.16	1.48	1.86	2.31	2.83	3.45	4.16	4.98	5.92	6.99
25		2.21	2.80	3.52	4.37	5.37	6.53	7.88	9.42	11.2	13.2
32		4.57	5.80	7.29	9.04	11.1	13.5	16.2	19.4	23.1	27.2
40		6.87	8.72	10.9	13.6	16.7	20.2	24.4	29.2	34.6	40.9
50		13.3	16.9	21.2	26.2	32.2	39.1	47.1	56.3	66.8	78.8
65		21.2	26.9	33.8	41.8	51.3	62.3	75.0	89.7	106	126
80		37.6	47.7	59.8	74.0	90.8	110	133	159	188	222
100		76.8	97.4	122	151	185	225	270	323	383	452

Note: (i) Capacity based on saturated vapour (no useful superheat)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 5c: Suction line capacities in kW for KLEA 407C
Saturated vapour leaving evaporator

Nominal line size mm	T $\Delta P/\Delta L$	Saturation temperature change 4.0 K in 100 m									
		Mean evaporating temperature °C at corresponding pressure drop, Pa/m									
		-40 192	-35 233	-30 278	-25 330	-20 387	-15 451	-10 522	-5 600	0 686	5 782
Type L Copper											
10	0.149	0.190	0.242	0.305	0.381	0.470	0.574	0.695	0.836	0.998	
12	0.345	0.440	0.560	0.705	0.878	1.08	1.32	1.60	1.92	2.29	
15	0.653	0.831	1.06	1.33	1.66	2.04	2.48	3.00	3.60	4.30	
19	1.12	1.42	1.81	2.28	2.83	3.48	4.24	5.12	6.15	7.32	
22	1.74	2.21	2.81	3.53	4.38	5.39	6.56	7.92	9.50	11.3	
28	3.54	4.50	5.72	7.18	8.91	10.9	13.3	16.1	19.2	22.9	
35	6.19	7.88	10.0	12.5	15.5	19.1	23.2	28.0	33.5	39.8	
42	9.81	12.5	15.9	19.9	24.6	30.2	36.7	44.2	52.9	62.9	
54	20.4	26.0	33.0	41.3	51.1	62.6	76.1	91.7	110	130	
67	36.2	46.1	58.4	73.1	90.4	111	134	162	193	230	
79	57.9	73.8	93.4	117	144	177	214	258	308	366	
92	86.2	110	139	174	215	263	319	383	458	543	
105	122	155	196	245	303	370	449	540	645	765	
Schedule 40 steel											
10	0.423	0.538	0.677	0.841	1.03	1.26	1.52	1.81	2.16	2.55	
15	0.788	1.00	1.26	1.56	1.92	2.33	2.81	3.37	4.00	4.72	
20	1.67	2.12	2.66	3.29	4.04	4.91	5.92	7.08	8.41	9.93	
25	3.16	4.01	5.03	6.24	7.65	9.30	11.2	13.4	15.9	18.8	
32	6.53	8.29	10.4	12.9	15.8	19.2	23.1	27.6	32.8	38.7	
40	9.81	12.4	15.6	19.3	23.7	28.8	34.6	41.4	49.1	58.0	
50	19.0	24.0	30.1	37.3	45.7	55.5	66.8	79.8	94.8	112	
65	30.3	38.4	48.1	59.5	72.9	88.5	107	127	151	178	
80	53.6	67.9	85.0	105	129	156	188	225	267	315	
100	109	138	173	214	263	319	383	458	543	641	

Note: (i) Capacity based on saturated vapour (no useful superheat)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 6a: Suction line capacities in kW for KLEA 407C
Suction line vapour with 5°C of superheat

Nominal line size mm	T ΔP/ΔL	Saturation temperature change 1.0 K in 100 m									
		Mean evaporating temperature °C at corresponding pressure drop, Pa/m									
		-40	-35	-30	-25	-20	-15	-10	-5	0	5
Type L Copper											
10	0.067	0.087	0.112	0.141	0.176	0.218	0.267	0.324	0.391	0.468	
12	0.157	0.203	0.260	0.328	0.409	0.505	0.618	0.750	0.902	1.08	
15	0.298	0.386	0.493	0.622	0.775	0.956	1.17	1.42	1.70	2.03	
19	0.513	0.664	0.847	1.07	1.33	1.64	2.00	2.42	2.91	3.48	
22	0.799	1.03	1.32	1.66	2.06	2.54	3.10	3.76	4.51	5.38	
28	1.64	2.12	2.69	3.39	4.21	5.19	6.32	7.65	9.18	10.9	
35	2.88	3.71	4.72	5.94	7.38	9.07	11.1	13.4	16.0	19.1	
42	4.58	5.90	7.51	9.43	11.7	14.4	17.5	21.2	25.4	30.3	
54	9.58	12.3	15.7	19.7	24.4	30.0	36.5	44.1	52.8	62.8	
67	17.0	21.9	27.9	34.9	43.3	53.2	64.7	78.0	93.4	111	
79	27.3	35.2	44.6	55.9	69.3	85.0	103	125	149	177	
92	40.8	52.5	66.5	83.3	103	127	154	186	222	264	
105	57.7	74.2	94.1	118	146	179	217	262	313	372	
Schedule 40 steel											
10	0.205	0.262	0.331	0.413	0.510	0.622	0.753	0.903	1.07	1.27	
15	0.383	0.490	0.619	0.771	0.950	1.16	1.40	1.68	2.00	2.36	
20	0.815	1.04	1.31	1.63	2.01	2.45	2.96	3.54	4.21	4.98	
25	1.55	1.98	2.49	3.10	3.81	4.64	5.60	6.71	7.98	9.42	
32	3.22	4.11	5.17	6.42	7.88	9.59	11.6	13.9	16.5	19.4	
40	4.85	6.18	7.77	9.65	11.8	14.4	17.4	20.8	24.7	29.2	
50	9.41	12.0	15.0	18.7	22.9	27.9	33.6	40.2	47.7	56.3	
65	15.0	19.1	24.0	29.8	36.6	44.5	53.6	64.1	76.1	89.8	
80	26.7	33.9	42.6	52.8	64.7	78.7	94.8	113	135	159	
100	54.6	69.3	86.9	108	132	160	193	231	274	323	

Note: (i) Capacity based on superheated vapour (superheat assumed useful)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 6b: Suction line capacities in kW for KLEA 407C
Suction line vapour with 5°C of superheat

Nominal line size mm	T ΔP/ΔL	Saturation temperature change 2.0 K in 100 m									
		Mean evaporating temperature °C at corresponding pressure drop, Pa/m									
		-40	-35	-30	-25	-20	-15	-10	-5	0	5
Type L Copper											
10	0.100	0.130	0.166	0.209	0.261	0.322	0.394	0.478	0.576	0.688	
12	0.232	0.301	0.384	0.485	0.604	0.745	0.910	1.10	1.33	1.58	
15	0.441	0.571	0.728	0.917	1.14	1.41	1.72	2.08	2.50	2.98	
19	0.758	0.980	1.25	1.57	1.95	2.41	2.94	3.55	4.26	5.08	
22	1.18	1.52	1.94	2.44	3.03	3.73	4.55	5.50	6.60	7.86	
28	2.41	3.11	3.96	4.97	6.17	7.59	9.25	11.2	13.4	15.9	
35	4.23	5.45	6.93	8.69	10.8	13.3	16.1	19.5	23.4	27.8	
42	6.72	8.66	11.0	13.8	17.1	21.0	25.6	30.9	37.0	44.0	
54	14.0	18.1	22.9	28.7	35.6	43.7	53.1	64.0	76.7	91.2	
67	24.9	32.0	40.6	50.9	63.1	77.3	94.0	113	136	161	
79	39.9	51.3	65.0	81.4	101	124	150	181	216	257	
92	59.6	76.5	96.9	121	150	184	223	269	321	382	
105	84.2	108	137	171	212	259	315	379	453	538	
Schedule 40 steel											
10	0.297	0.379	0.478	0.595	0.732	0.892	1.08	1.29	1.54	1.81	
15	0.554	0.707	0.890	1.11	1.36	1.66	2.00	2.40	2.85	3.37	
20	1.17	1.50	1.88	2.34	2.87	3.50	4.22	5.05	6.00	7.09	
25	2.23	2.84	3.57	4.44	5.45	6.63	7.99	9.56	11.4	13.4	
32	4.63	5.89	7.39	9.17	11.3	13.7	16.5	19.7	23.4	27.6	
40	6.96	8.85	11.1	13.8	16.9	20.5	24.7	29.6	35.1	41.4	
50	13.5	17.1	21.5	26.6	32.6	39.6	47.7	57.1	67.7	79.9	
65	21.5	27.3	34.3	42.5	52.1	63.2	76.1	91.0	108	127	
80	38.1	48.4	60.7	75.1	92.1	112	135	161	191	225	
100	77.8	98.8	124	153	188	228	274	328	389	459	

Note: (i) Capacity based on superheated vapour (superheat assumed useful)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 6c: Suction line capacities in kW for KLEA 407C
Suction line vapour with 5°C of superheat

Nominal line size mm	T $\Delta P/\Delta L$	Saturation temperature change 4.0 K in 100 m									
		Mean evaporating temperature °C at corresponding pressure drop, Pa/m									
		-40 192	-35 233	-30 278	-25 330	-20 387	-15 451	-10 522	-5 600	0 686	5 782
Type L Copper											
10	0.148	0.192	0.245	0.309	0.385	0.475	0.581	0.704	0.846	1.01	
12	0.344	0.445	0.567	0.714	0.889	1.10	1.34	1.62	1.94	2.32	
15	0.651	0.841	1.07	1.35	1.68	2.06	2.52	3.04	3.65	4.35	
19	1.12	1.44	1.84	2.31	2.87	3.52	4.29	5.19	6.22	7.41	
22	1.74	2.24	2.85	3.57	4.44	5.46	6.64	8.02	9.62	11.4	
28	3.54	4.56	5.79	7.27	9.02	11.1	13.5	16.3	19.5	23.2	
35	6.20	7.98	10.1	12.7	15.7	19.3	23.5	28.3	33.9	40.3	
42	9.84	12.7	16.1	20.1	24.9	30.6	37.2	44.8	53.6	63.7	
54	20.5	26.4	33.4	41.8	51.8	63.5	77.1	92.8	111	132	
67	36.4	46.7	59.2	74.0	91.6	112	136	164	196	233	
79	58.2	74.7	94.6	118	146	179	217	261	312	371	
92	86.7	111	141	176	218	266	323	388	464	550	
105	123	157	199	248	307	375	455	547	653	775	
Schedule 40 steel											
10	0.428	0.546	0.686	0.853	1.05	1.27	1.54	1.84	2.19	2.58	
15	0.797	1.02	1.28	1.58	1.95	2.37	2.85	3.41	4.05	4.79	
20	1.69	2.15	2.69	3.34	4.10	4.99	6.01	7.18	8.53	10.1	
25	3.20	4.07	5.10	6.33	7.76	9.43	11.4	13.6	16.1	19.0	
32	6.62	8.41	10.5	13.1	16.0	19.5	23.4	28.0	33.2	39.2	
40	9.94	12.6	15.8	19.6	24.0	29.2	35.1	42.0	49.9	58.8	
50	19.2	24.4	30.6	37.8	46.4	56.3	67.8	81.0	96.1	113	
65	30.7	38.9	48.8	60.4	74.0	89.8	108	129	153	181	
80	54.3	68.9	86.3	107	131	159	191	228	271	319	
100	111	140	176	218	266	323	389	464	551	650	

Note: (i) Capacity based on superheated vapour (superheat assumed useful)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 7a: Suction line capacities in kW for KLEA 407C
Suction line vapour at 20°C

Nominal line size mm	T $\Delta P/\Delta L$	Saturation temperature change 1.0 K in 100 m									
		Mean evaporating temperature °C at corresponding pressure drop, Pa/m									
		-40 48	-35 58	-30 70	-25 82	-20 97	-15 113	-10 130	-5 150	0 172	5 195
Type L Copper											
10		0.056	0.073	0.096	0.123	0.156	0.196	0.243	0.299	0.366	0.444
12		0.130	0.172	0.223	0.286	0.363	0.454	0.563	0.693	0.846	1.03
15		0.249	0.328	0.425	0.544	0.688	0.860	1.07	1.31	1.60	1.93
19		0.429	0.564	0.731	0.935	1.18	1.48	1.83	2.24	2.73	3.31
22		0.669	0.880	1.14	1.45	1.84	2.29	2.84	3.48	4.23	5.12
28		1.38	1.80	2.33	2.98	3.75	4.68	5.78	7.08	8.62	10.4
35		2.42	3.17	4.10	5.22	6.57	8.19	10.1	12.4	15.1	18.2
42		3.86	5.05	6.52	8.30	10.4	13.0	16.1	19.6	23.9	28.8
54		8.09	10.6	13.6	17.3	21.8	27.1	33.4	40.9	49.6	59.8
67		14.4	18.8	24.2	30.8	38.7	48.1	59.3	72.4	87.8	106
79		23.1	30.2	38.9	49.4	62.0	77.0	94.8	116	140	169
92		34.6	45.1	58.0	73.6	92.4	115	141	172	209	252
105		49.0	63.8	82.0	104	131	162	199	243	295	355
Schedule 40 steel											
10		0.174	0.227	0.291	0.367	0.459	0.567	0.694	0.842	1.01	1.21
15		0.327	0.425	0.544	0.686	0.856	1.06	1.29	1.57	1.88	2.26
20		0.697	0.904	1.15	1.46	1.81	2.23	2.73	3.31	3.98	4.76
25		1.33	1.72	2.20	2.77	3.44	4.24	5.18	6.27	7.53	9.00
32		2.77	3.58	4.56	5.74	7.13	8.77	10.7	12.9	15.6	18.6
40		4.18	5.39	6.87	8.63	10.7	13.2	16.1	19.4	23.3	27.9
50		8.11	10.5	13.3	16.7	20.7	25.5	31.1	37.5	45.1	53.8
65		13.0	16.7	21.3	26.7	33.1	40.7	49.6	59.9	71.9	85.8
80		23.1	29.7	37.7	47.3	58.7	72.1	87.7	106	127	152
100		47.3	60.8	77.1	96.6	120	147	179	216	259	309

Note: (i) Capacity based on saturated vapour (no useful superheat)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 7b: Suction line capacities in kW for KLEA 407C
Suction line vapour at 20°C

Nominal line size mm	T $\Delta P/\Delta L$	Saturation temperature change 2.0 K in 100 m									
		Mean evaporating temperature °C at corresponding pressure drop, Pa/m									
		-40 96	-35 116	-30 139	-25 165	-20 193	-15 225	-10 261	-5 300	0 343	5 391
Type L Copper											
10		0.083	0.110	0.142	0.183	0.231	0.290	0.359	0.442	0.540	0.654
12		0.194	0.256	0.331	0.424	0.536	0.671	0.830	1.02	1.24	1.51
15		0.369	0.485	0.629	0.803	1.01	1.27	1.57	1.92	2.34	2.83
19		0.636	0.835	1.08	1.38	1.74	2.17	2.68	3.29	4.00	4.84
22		0.990	1.30	1.68	2.14	2.70	3.37	4.16	5.09	6.19	7.48
28		2.03	2.66	3.43	4.37	5.50	6.86	8.46	10.4	12.6	15.2
35		3.56	4.66	6.02	7.66	9.63	12.0	14.8	18.1	21.9	26.5
42		5.67	7.42	9.56	12.2	15.3	19.0	23.4	28.6	34.7	41.9
54		11.9	15.5	20.0	25.3	31.8	39.6	48.7	59.5	72.1	86.9
67		21.1	27.6	35.4	45.0	56.4	70.1	86.2	105	127	153
79		33.9	44.2	56.7	72.0	90.3	112	138	168	203	245
92		50.6	65.9	84.6	107	134	167	205	250	302	364
105		71.5	93.2	120	152	190	235	289	353	427	513
Schedule 40 steel											
10		0.254	0.329	0.421	0.530	0.661	0.814	0.995	1.21	1.45	1.73
15		0.475	0.615	0.785	0.988	1.23	1.51	1.85	2.24	2.69	3.22
20		1.01	1.31	1.66	2.09	2.60	3.20	3.90	4.72	5.67	6.77
25		1.92	2.48	3.16	3.97	4.93	6.06	7.39	8.93	10.7	12.8
32		3.99	5.15	6.54	8.21	10.2	12.5	15.2	18.4	22.1	26.4
40		6.01	7.74	9.84	12.3	15.3	18.8	22.9	27.7	33.2	39.6
50		11.7	15.0	19.0	23.9	29.6	36.3	44.2	53.4	64.0	76.4
65		18.6	24.0	30.4	38.1	47.2	57.9	70.5	85.1	102	122
80		33.1	42.5	53.9	67.5	83.6	103	125	151	181	215
100		67.6	86.8	110	138	170	209	254	307	368	438

Note: (i) Capacity based on saturated vapour (no useful superheat)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 7c: Suction line capacities in kW for KLEA 407C
Suction line vapour at 20°C

Nominal line size mm	T $\Delta P/\Delta L$	Saturation temperature change 4.0 K in 100 m Mean evaporating temperature °C at corresponding pressure drop, Pa/m									
		-40 192	-35 233	-30 278	-25 330	-20 387	-15 451	-10 522	-5 600	0 686	5 782
		Type L Copper									
10	0.124	0.163	0.211	0.271	0.342	0.428	0.530	0.651	0.793	0.960	
12	0.288	0.379	0.490	0.626	0.791	0.987	1.22	1.50	1.82	2.20	
15	0.547	0.717	0.928	1.18	1.49	1.86	2.30	2.82	3.43	4.14	
19	0.939	1.23	1.59	2.03	2.55	3.18	3.93	4.81	5.84	7.06	
22	1.46	1.91	2.47	3.15	3.96	4.93	6.08	7.44	9.03	10.9	
28	2.99	3.91	5.04	6.41	8.05	10.0	12.3	15.1	18.3	22.1	
35	5.24	6.84	8.81	11.2	14.1	17.5	21.5	26.3	31.9	38.4	
42	8.33	10.9	14.0	17.8	22.3	27.7	34.1	41.6	50.4	60.7	
54	17.4	22.7	29.1	37.0	46.4	57.5	70.8	86.3	104	126	
67	30.9	40.2	51.7	65.5	82.1	102	125	152	184	222	
79	49.5	64.4	82.7	105	131	163	200	243	294	353	
92	73.8	96.0	123	156	195	242	297	361	437	525	
105	104	136	174	220	275	341	419	509	616	739	
Schedule 40 steel											
10	0.368	0.476	0.606	0.762	0.947	1.17	1.42	1.72	2.07	2.47	
15	0.686	0.887	1.13	1.42	1.76	2.16	2.64	3.19	3.83	4.57	
20	1.46	1.88	2.39	2.99	3.72	4.56	5.56	6.72	8.06	9.63	
25	2.77	3.56	4.53	5.67	7.04	8.64	10.5	12.7	15.2	18.2	
32	5.73	7.37	9.35	11.7	14.5	17.8	21.7	26.2	31.4	37.5	
40	8.62	11.1	14.1	17.6	21.8	26.8	32.5	39.3	47.1	56.2	
50	16.7	21.4	27.2	34.0	42.1	51.6	62.8	75.8	90.9	108	
65	26.7	34.2	43.4	54.2	67.2	82.3	100	121	145	173	
80	47.2	60.6	76.7	96.0	119	146	177	214	256	305	
100	96.4	124	156	196	242	297	360	435	521	621	

Note: (i) Capacity based on saturated vapour (no useful superheat)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 8a: Discharge line capacities in kW for KLEA 407C

Nominal line size mm	Condenser saturation temperature drop 2.0 K in 100 m Mean evaporating temperature °C						Pressure gradient of 836 Pa/m Discharge line superheat of 45.0 K			
	T	-40.0	-35.0	-30.0	-25.0	-20.0	-15.0	-10.0	-5.0	0.0
Type L Copper										
10	1.31	1.34	1.37	1.40	1.43	1.46	1.49	1.52	1.55	1.57
12	2.99	3.06	3.13	3.21	3.28	3.34	3.41	3.48	3.54	3.60
15	5.60	5.74	5.88	6.01	6.14	6.27	6.40	6.52	6.64	6.75
19	9.54	9.77	10.0	10.2	10.5	10.7	10.9	11.1	11.3	11.5
22	14.7	15.1	15.4	15.8	16.1	16.5	16.8	17.1	17.4	17.7
28	29.8	30.5	31.2	31.9	32.6	33.3	34.0	34.6	35.3	35.9
35	51.7	53.0	54.3	55.5	56.7	57.9	59.1	60.2	61.3	62.4
42	81.7	83.7	85.7	87.6	89.5	91.4	93.3	95.0	96.8	98.5
54	169	173	177	181	185	189	193	196	200	203
67	298	305	312	319	326	333	340	346	353	359
79	474	485	497	508	519	530	541	551	561	571
92	703	720	737	754	770	786	802	818	833	847
105	989	1014	1038	1061	1084	1107	1129	1151	1172	1192
Schedule 40 steel										
10	3.27	3.35	3.43	3.51	3.59	3.66	3.73	3.81	3.88	3.94
15	6.06	6.21	6.36	6.50	6.64	6.78	6.92	7.05	7.18	7.30
20	12.7	13.1	13.4	13.7	14.0	14.3	14.5	14.8	15.1	15.4
25	24.1	24.7	25.3	25.8	26.4	26.9	27.5	28.0	28.5	29.0
32	49.6	50.8	52.0	53.2	54.3	55.5	56.6	57.7	58.7	59.8
40	74.4	76.2	78.0	79.8	81.5	83.2	84.9	86.5	88.1	89.6
50	143	147	150	154	157	160	164	167	170	173
65	228	234	239	245	250	256	261	266	270	275
80	403	413	423	433	442	451	460	469	478	486
100	821	841	861	880	900	918	937	955	972	989

Note: (i) Capacity based on saturated vapour (no useful superheat)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 8b: Discharge line capacities in kW for KLEA 407C

Nominal line size mm	Condenser saturation temperature change 2.0 K in 100 m Mean evaporating temperature °C						Pressure gradient of 836 Pa/m Discharge line superheat of 60.0 K			
	T	-40.0	-35.0	-30.0	-25.0	-20.0	-15.0	-10.0	-5.0	0.0
Type L Copper										
10	1.26	1.29	1.32	1.35	1.38	1.40	1.43	1.46	1.49	1.51
12	2.88	2.95	3.02	3.08	3.15	3.22	3.28	3.35	3.41	3.47
15	5.40	5.53	5.66	5.79	5.91	6.04	6.16	6.28	6.39	6.50
19	9.19	9.41	9.63	9.85	10.1	10.3	10.5	10.7	10.9	11.1
22	14.2	14.5	14.9	15.2	15.5	15.9	16.2	16.5	16.8	17.1
28	28.7	29.4	30.1	30.8	31.4	32.1	32.7	33.4	34.0	34.6
35	49.9	51.1	52.3	53.5	54.7	55.8	56.9	58.0	59.1	60.1
42	78.8	80.7	82.6	84.5	86.3	88.1	89.9	91.6	93.3	94.9
54	163	167	171	175	178	182	186	189	193	196
67	287	294	301	308	315	321	328	334	340	346
79	457	468	479	490	501	512	522	532	542	551
92	678	695	711	728	743	759	774	789	804	817
105	955	979	1002	1024	1047	1069	1090	1111	1131	1151
Schedule 40 steel										
10	3.17	3.24	3.32	3.39	3.47	3.54	3.61	3.68	3.75	3.81
15	5.86	6.01	6.15	6.29	6.43	6.56	6.69	6.82	6.95	7.07
20	12.3	12.6	12.9	13.2	13.5	13.8	14.1	14.3	14.6	14.9
25	23.3	23.9	24.4	25.0	25.5	26.1	26.6	27.1	27.6	28.1
32	48.0	49.2	50.3	51.5	52.6	53.7	54.8	55.8	56.9	57.8
40	72.0	73.7	75.5	77.2	78.9	80.5	82.2	83.7	85.3	86.7
50	139	142	145	149	152	155	158	161	164	167
65	221	226	232	237	242	247	252	257	262	266
80	390	400	409	419	428	437	446	454	463	471
100	795	814	833	852	871	889	907	924	941	958

Note: (i) Capacity based on saturated vapour (no useful superheat)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 9a: Liquid line capacities in kW for KLEA 407C

Nominal line size mm	T	Liquid line velocity 0.5 m/s Mean evaporating temperature °C								
		-40.0	-35.0	-30.0	-25.0	-20.0	-15.0	-10.0	-5.0	0.0
Type L Copper										
10	3.59	3.67	3.76	3.85	3.93	4.01	4.09	4.17	4.25	4.32
12	6.68	6.84	7.01	7.17	7.32	7.48	7.63	7.77	7.91	8.05
15	10.7	11.0	11.3	11.5	11.8	12.0	12.2	12.5	12.7	12.9
19	16.0	16.4	16.8	17.2	17.6	17.9	18.3	18.7	19.0	19.3
22	22.3	22.8	23.4	23.9	24.4	24.9	25.4	25.9	26.4	26.8
28	38.0	38.9	39.8	40.7	41.6	42.5	43.4	44.2	45.0	45.8
35	57.8	59.3	60.7	62.0	63.4	64.7	66.0	67.3	68.5	69.7
42	81.9	83.9	85.9	87.8	89.7	91.6	93.5	95.3	97.0	98.7
54	142	146	149	153	156	159	163	166	169	172
67	220	225	230	236	241	246	251	255	260	265
79	313	321	329	336	344	351	358	365	371	378
92	424	434	445	455	465	474	484	493	502	511
105	551	565	578	591	604	617	629	641	653	664
Schedule 40 steel										
10	8.78	9.00	9.21	9.42	9.62	9.83	10.0	10.2	10.4	10.6
15	14.0	14.3	14.7	15.0	15.3	15.6	16.0	16.3	16.6	16.9
20	24.5	25.1	25.7	26.3	26.9	27.5	28.0	28.6	29.1	29.6
25	39.8	40.7	41.7	42.6	43.6	44.5	45.4	46.3	47.1	47.9
32	68.8	70.5	72.2	73.8	75.4	77.0	78.6	80.1	81.5	82.9
40	93.7	96.0	98.2	100	103	105	107	109	111	113
50	154	158	162	166	169	173	176	180	183	186
65	220	226	231	236	241	247	251	256	261	266
80	340	349	357	365	373	381	388	396	403	410
100	586	600	614	628	642	656	669	682	694	706

Note: (i) Capacity based on saturated vapour (no useful superheat)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

Table 9b: Liquid line capacities in kW for KLEA 407C

Nominal line size mm	T	Condenser saturation temperature change 2.0 K in 100 m Mean evaporating temperature °C								
		-40.0	-35.0	-30.0	-25.0	-20.0	-15.0	-10.0	-5.0	0.0
Type L Copper										
10	5.42	5.55	5.68	5.81	5.94	6.06	6.18	6.30	6.42	6.53
12	12.5	12.8	13.1	13.4	13.7	13.9	14.2	14.5	14.8	15.0
15	23.5	24.0	24.6	25.2	25.7	26.3	26.8	27.3	27.8	28.3
19	40.1	41.0	42.0	43.0	43.9	44.8	45.7	46.6	47.5	48.3
22	62.0	63.5	65.0	66.5	67.9	69.4	70.8	72.1	73.4	74.7
28	126	129	132	135	138	141	144	146	149	152
35	219	225	230	235	240	245	250	255	260	264
42	347	355	364	372	380	388	396	404	411	418
54	719	737	754	772	788	805	821	837	852	867
67	1271	1302	1333	1364	1393	1423	1451	1479	1506	1532
79	2028	2078	2127	2175	2223	2269	2315	2359	2402	2444
92	3014	3088	3161	3232	3303	3372	3440	3506	3570	3632
105	4249	4353	4456	4557	4657	4754	4850	4943	5033	5120
Schedule 40 steel										
10	14.4	14.7	15.1	15.4	15.7	16.1	16.4	16.7	17.0	17.3
15	26.7	27.3	28.0	28.6	29.2	29.8	30.4	31.0	31.6	32.1
20	56.1	57.5	58.9	60.2	61.5	62.8	64.1	65.3	66.5	67.6
25	106	109	111	114	116	119	121	124	126	128
32	219	224	230	235	240	245	250	255	259	264
40	328	336	344	352	360	367	375	382	389	396
50	633	649	664	679	694	709	723	737	750	763
65	1010	1035	1059	1083	1107	1130	1153	1175	1196	1217
80	1785	1828	1872	1914	1956	1997	2037	2076	2114	2151
100	3634	3723	3811	3898	3983	4066	4148	4228	4305	4379

Note: (i) Capacity based on saturated vapour (no useful superheat)
(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

**Table 10a: Minimum refrigeration capacities in kW for KLEA 407C
Lubricant is EMKARATE RL™ 32S**
Type L Copper Tubing

Evap. temp. °C	Suction temp. °C	Nominal line size mm	10	12	15	19	22	28	35	42	54	67	79	92	105
0	10		0.266	0.580	1.05	1.73	2.61	5.09	8.61	13.3	26.6	45.6	71.2	104	144
	15		0.263	0.572	1.03	1.71	2.58	5.02	8.49	13.1	26.2	45.0	70.2	102	142
	20		0.259	0.564	1.02	1.69	2.54	4.95	8.38	12.9	25.8	44.4	69.3	101	140
	5		0.242	0.528	0.954	1.58	2.38	4.63	7.84	12.1	24.2	41.5	64.8	94.5	131
	10		0.239	0.520	0.941	1.56	2.35	4.57	7.73	11.9	23.8	41.0	63.9	93.2	129
	15		0.236	0.514	0.929	1.53	2.31	4.51	7.63	11.8	23.5	40.4	63.1	92.0	128
-5	0		0.220	0.478	0.865	1.43	2.16	4.20	7.10	11.0	21.9	37.7	58.8	85.7	119
	5		0.217	0.472	0.854	1.41	2.13	4.14	7.01	10.8	21.6	37.2	58.0	84.6	117
	10		0.214	0.466	0.842	1.39	2.10	4.09	6.92	10.7	21.3	36.7	57.2	83.5	116
-10	-5		0.199	0.432	0.781	1.29	1.95	3.79	6.42	9.91	19.8	34.0	53.1	77.4	107
	0		0.196	0.426	0.771	1.27	1.92	3.74	6.33	9.78	19.5	33.6	52.4	76.4	106
	5		0.193	0.421	0.761	1.26	1.90	3.70	6.25	9.65	19.3	33.1	51.7	75.4	105
-15	-10		0.179	0.389	0.703	1.16	1.75	3.41	5.77	8.91	17.8	30.6	47.7	69.6	96.6
	-5		0.176	0.384	0.694	1.15	1.73	3.37	5.69	8.79	17.6	30.2	47.1	68.7	95.4
	0		0.174	0.379	0.685	1.13	1.71	3.32	5.62	8.68	17.3	29.8	46.5	67.8	94.1
-20	-15		0.160	0.348	0.629	1.04	1.57	3.05	5.17	7.98	15.9	27.4	42.7	62.3	86.5
	-10		0.158	0.343	0.621	1.03	1.55	3.01	5.10	7.87	15.7	27.0	42.2	61.5	85.4
	-5		0.156	0.339	0.613	1.01	1.53	2.98	5.03	7.77	15.5	26.7	41.6	60.7	84.3
-25	-20		0.142	0.310	0.560	0.926	1.40	2.72	4.60	7.10	14.2	24.4	38.0	55.5	77.0
	-15		0.140	0.306	0.553	0.914	1.38	2.68	4.54	7.01	14.0	24.1	37.5	54.8	76.0
	-10		0.139	0.302	0.546	0.902	1.36	2.65	4.48	6.92	13.8	23.8	37.1	54.1	75.1
-30	-25		0.126	0.274	0.496	0.820	1.24	2.41	4.07	6.29	12.6	21.6	33.7	49.2	68.2
	-20		0.124	0.271	0.490	0.809	1.22	2.38	4.02	6.21	12.4	21.3	33.3	48.5	67.3
	-15		0.123	0.267	0.483	0.799	1.20	2.35	3.97	6.13	12.2	21.0	32.8	47.9	66.5
-35	-30		0.111	0.242	0.437	0.722	1.09	2.12	3.59	5.54	11.1	19.0	29.7	43.3	60.1
	-25		0.110	0.238	0.431	0.712	1.07	2.09	3.54	5.47	10.9	18.8	29.3	42.7	59.3
	-20		0.108	0.235	0.426	0.703	1.06	2.07	3.49	5.40	10.8	18.5	28.9	42.2	58.5
-40	-35		0.097	0.211	0.382	0.631	0.952	1.85	3.14	4.84	9.67	16.6	25.9	37.8	52.5
	-30		0.096	0.208	0.377	0.623	0.939	1.83	3.10	4.78	9.55	16.4	25.6	37.3	51.8
	-25		0.095	0.206	0.372	0.615	0.927	1.81	3.06	4.72	9.43	16.2	25.3	36.9	51.2

- (i) Capacity based on saturated vapour (no useful superheat)
- (ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C
- (iii) Content of refrigerant in lubricant estimated from solubility data at suction gas temperature and pressure

**Table 10b: Minimum refrigeration capacities in kW for KLEA 407C
Lubricant is EMKARATE RL™ 32S**
Schedule 40 Steel Pipe

Evap. temp. °C	Suction temp. °C	Nominal line size mm	10	15	20	25	32	40	50	65	80	100
0	10		0.816	1.46	2.95	5.39	10.7	15.7	29.4	45.8	78.9	156
	15		0.805	1.44	2.91	5.32	10.6	15.5	29.0	45.2	77.8	153
	20		0.794	1.42	2.87	5.24	10.4	15.3	28.6	44.6	76.7	151
	5		0.743	1.33	2.68	4.90	9.74	14.3	26.7	41.7	71.8	142
	10		0.733	1.31	2.65	4.84	9.61	14.1	26.4	41.1	70.8	140
	15		0.723	1.29	2.61	4.77	9.48	13.9	26.0	40.6	69.9	138
-5	0		0.673	1.20	2.43	4.45	8.83	13.0	24.2	37.8	65.1	128
	5		0.664	1.19	2.40	4.39	8.71	12.8	23.9	37.3	64.2	127
	10		0.656	1.17	2.37	4.33	8.60	12.6	23.6	36.8	63.4	125
-10	-5		0.608	1.09	2.20	4.02	7.98	11.7	21.9	34.1	58.8	116
	0		0.600	1.07	2.17	3.96	7.87	11.6	21.6	33.7	58.0	114
	5		0.592	1.06	2.14	3.91	7.77	11.4	21.3	33.3	57.3	113
-15	-10		0.547	0.979	1.98	3.61	7.17	10.5	19.7	30.7	52.9	104
	-5		0.540	0.966	1.95	3.56	7.08	10.4	19.4	30.3	52.2	103
	0		0.533	0.953	1.93	3.52	6.99	10.3	19.2	29.9	51.5	102
-20	-15		0.490	0.876	1.77	3.23	6.42	9.44	17.6	27.5	47.3	93.3
	-10		0.483	0.865	1.75	3.19	6.34	9.31	17.4	27.1	46.7	92.1
	-5		0.477	0.854	1.72	3.15	6.26	9.20	17.2	26.8	46.1	91.0
-25	-20		0.436	0.780	1.58	2.88	5.72	8.41	15.7	24.5	42.1	83.1
	-15		0.430	0.770	1.56	2.84	5.64	8.30	15.5	24.2	41.6	82.1
	-10		0.425	0.760	1.54	2.81	5.57	8.19	15.3	23.9	41.1	81.0
-30	-25		0.386	0.691	1.40	2.55	5.06	7.44	13.9	21.7	37.3	73.6
	-20		0.381	0.682	1.38	2.52	5.00	7.35	13.7	21.4	36.8	72.7
	-15		0.376	0.673	1.36	2.49	4.93	7.25	13.6	21.1	36.4	71.7
-35	-30		0.340	0.608	1.23	2.25	4.46	6.55	12.2	19.1	32.9	64.8
	-25		0.336	0.600	1.21	2.22	4.40	6.47	12.1	18.8	32.4	64.0
	-20		0.331	0.593	1.20	2.19	4.34	6.39	11.9	18.6	32.0	63.2
-40	-35		0.297	0.532	1.07	1.96	3.90	5.73	10.7	16.7	28.7	56.7
	-30		0.293	0.525	1.06	1.94	3.85	5.66	10.6	16.5	28.4	55.9
	-25		0.290	0.518	1.05	1.91	3.80	5.58	10.4	16.3	28.0	55.2

- (i) Capacity based on saturated vapour (no useful superheat)
- (ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C
- (iii) Content of refrigerant in lubricant estimated from solubility data at suction gas temperature and pressure

Table 10c: Minimum refrigeration capacities in kW for KLEA 407C**Lubricant is EMKARATE RL™ 68S****Type L Copper Tubing**

Evap. temp. °C	Suction temp. °C	Nominal line size mm	10	12	15	19	22	28	35	42	54	67	79	92	105
0	5	0.243	0.529	0.957	1.58	2.38	4.65	7.86	12.1	24.2	41.6	65.0	94.8	132	
	10	0.240	0.522	0.944	1.56	2.35	4.58	7.75	12.0	23.9	41.1	64.1	93.5	130	
	15	0.237	0.515	0.931	1.54	2.32	4.52	7.65	11.8	23.6	40.5	63.2	92.2	128	
	-5	0.220	0.480	0.867	1.43	2.16	4.21	7.12	11.0	22.0	37.8	58.9	85.9	119	
	5	0.217	0.473	0.856	1.41	2.13	4.16	7.03	10.9	21.7	37.3	58.1	84.8	118	
	10	0.215	0.467	0.845	1.40	2.10	4.10	6.94	10.7	21.4	36.8	57.4	83.7	116	
	-10	0.199	0.433	0.784	1.29	1.95	3.80	6.43	9.94	19.8	34.1	53.2	77.6	108	
	0	0.196	0.428	0.773	1.28	1.93	3.75	6.35	9.80	19.6	33.7	52.5	76.6	106	
	5	0.194	0.422	0.763	1.26	1.90	3.71	6.27	9.68	19.3	33.2	51.8	75.6	105	
-15	-10	0.179	0.390	0.705	1.16	1.76	3.42	5.79	8.94	17.9	30.7	47.9	69.8	96.9	
	-5	0.177	0.385	0.695	1.15	1.73	3.38	5.71	8.82	17.6	30.3	47.2	68.9	95.6	
	0	0.174	0.380	0.687	1.13	1.71	3.33	5.64	8.71	17.4	29.9	46.6	68.0	94.4	
	-20	0.160	0.349	0.631	1.04	1.57	3.06	5.18	8.00	16.0	27.5	42.8	62.5	86.7	
	-10	0.158	0.344	0.623	1.03	1.55	3.02	5.11	7.90	15.8	27.1	42.3	61.7	85.6	
	-5	0.156	0.340	0.615	1.02	1.53	2.98	5.05	7.80	15.6	26.8	41.7	60.9	84.5	
	-25	0.143	0.311	0.562	0.928	1.40	2.73	4.61	7.12	14.2	24.5	38.2	55.7	77.3	
	-15	0.141	0.307	0.555	0.916	1.38	2.69	4.55	7.03	14.0	24.1	37.7	54.9	76.3	
	-10	0.139	0.303	0.548	0.905	1.36	2.66	4.50	6.94	13.9	23.8	37.2	54.2	75.3	
-30	-25	0.126	0.275	0.498	0.822	1.24	2.42	4.09	6.31	12.6	21.7	33.8	49.3	68.4	
	-20	0.125	0.272	0.491	0.812	1.22	2.38	4.03	6.23	12.4	21.4	33.4	48.7	67.5	
	-15	0.123	0.268	0.485	0.801	1.21	2.35	3.98	6.15	12.3	21.1	32.9	48.0	66.7	
	-35	0.111	0.242	0.438	0.724	1.09	2.13	3.60	5.55	11.1	19.1	29.7	43.4	60.2	
	-25	0.110	0.239	0.432	0.714	1.08	2.10	3.55	5.48	11.0	18.8	29.4	42.8	59.4	
	-20	0.108	0.236	0.427	0.705	1.06	2.07	3.51	5.41	10.8	18.6	29.0	42.3	58.7	
	-40	0.097	0.212	0.383	0.633	0.954	1.86	3.14	4.86	9.70	16.7	26.0	37.9	52.7	
	-35	0.096	0.209	0.378	0.625	0.942	1.84	3.10	4.79	9.58	16.5	25.7	37.4	52.0	
	-25	0.095	0.206	0.373	0.617	0.930	1.81	3.06	4.73	9.45	16.2	25.3	37.0	51.3	

(i) Capacity based on saturated vapour (no useful superheat)

(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

(iii) Content of refrigerant in lubricant estimated from solubility data at suction gas temperature and pressure

Table 10d: Minimum refrigeration capacities in kW for KLEA 407C**Lubricant is EMKARATE RL™ 68S****Schedule 40 Steel Pipe**

Evap. temp. °C	Suction temp. °C	Nominal line size mm	10	15	20	25	32	40	50	65	80	100
0	5	0.745	1.33	2.69	4.92	9.76	14.4	26.8	41.8	72.0	142	
	10	0.734	1.31	2.65	4.85	9.63	14.2	26.4	41.2	71.0	140	
	15	0.725	1.30	2.62	4.79	9.50	14.0	26.1	40.7	70.0	138	
	-5	0.675	1.21	2.44	4.46	8.85	13.0	24.3	37.9	65.3	129	
	5	0.666	1.19	2.41	4.40	8.74	12.8	24.0	37.4	64.4	127	
	10	0.657	1.18	2.38	4.34	8.62	12.7	23.7	36.9	63.5	125	
	-10	0.610	1.09	2.20	4.03	8.00	11.8	22.0	34.2	59.0	116	
	0	0.602	1.08	2.17	3.97	7.89	11.6	21.7	33.8	58.2	115	
	5	0.594	1.06	2.15	3.92	7.79	11.5	21.4	33.4	57.4	113	
-15	-10	0.548	0.981	1.98	3.62	7.19	10.6	19.7	30.8	53.0	105	
	-5	0.541	0.968	1.96	3.57	7.10	10.4	19.5	30.4	52.3	103	
	0	0.534	0.956	1.93	3.53	7.01	10.3	19.2	30.0	51.7	102	
	-20	0.491	0.878	1.77	3.24	6.44	9.46	17.7	27.6	47.5	93.6	
	-10	0.485	0.867	1.75	3.20	6.35	9.34	17.4	27.2	46.8	92.4	
	-5	0.478	0.856	1.73	3.16	6.27	9.22	17.2	26.9	46.2	91.2	
	-25	0.437	0.782	1.58	2.89	5.73	8.43	15.7	24.6	42.3	83.4	
	-15	0.432	0.772	1.56	2.85	5.66	8.32	15.5	24.2	41.7	82.3	
	-10	0.426	0.762	1.54	2.81	5.59	8.21	15.3	23.9	41.2	81.2	
-30	-25	0.387	0.693	1.40	2.56	5.08	7.47	13.9	21.7	37.4	73.8	
	-20	0.382	0.684	1.38	2.52	5.01	7.37	13.8	21.5	36.9	72.9	
	-15	0.377	0.675	1.36	2.49	4.95	7.28	13.6	21.2	36.5	72.0	
	-30	0.341	0.610	1.23	2.25	4.47	6.57	12.3	19.1	33.0	65.0	
	-25	0.336	0.602	1.22	2.22	4.41	6.49	12.1	18.9	32.5	64.2	
	-20	0.332	0.594	1.20	2.19	4.36	6.40	12.0	18.7	32.1	63.3	
	-40	0.298	0.533	1.08	1.97	3.91	5.75	10.7	16.7	28.8	56.8	
	-30	0.294	0.526	1.06	1.94	3.86	5.67	10.6	16.5	28.4	56.1	
	-25	0.290	0.520	1.05	1.92	3.81	5.60	10.5	16.3	28.1	55.4	

(i) Capacity based on saturated vapour (no useful superheat)

(ii) Mean condenser temperature 40 °C (no subcooling) i.e. liquid temperature of 37.4 °C

(iii) Content of refrigerant in lubricant estimated from solubility data at suction gas temperature and pressure

Table I 1a: Suction line capacity correction factors for KLEA 407C

To convert from tabulated values at a mean condenser temperature of 40°C to the desired value, multiply by the appropriate factor.

Evap. Temp. °C	Temperature liquid °C							
	20	25	30	35	37.4	40	45	50
5	1.176	1.127	1.077	1.026	1.000	0.972	0.917	0.859
0	1.179	1.130	1.079	1.026	1.000	0.972	0.915	0.856
-5	1.182	1.132	1.080	1.027	1.000	0.971	0.914	0.854
-10	1.186	1.134	1.082	1.027	1.000	0.971	0.912	0.851
-15	1.190	1.137	1.083	1.028	1.000	0.970	0.910	0.848
-20	1.194	1.140	1.085	1.028	1.000	0.970	0.908	0.845
-25	1.198	1.143	1.087	1.029	1.000	0.969	0.906	0.841
-30	1.203	1.146	1.089	1.030	1.000	0.968	0.904	0.838
-35	1.207	1.150	1.091	1.030	1.000	0.967	0.902	0.834
-40	1.212	1.154	1.093	1.031	1.000	0.967	0.900	0.830

Note: liquid temperature at a mean condensing temperature of 40.0 °C is 37.4 °C
hence table is referenced to a liquid temperature of 37.4 °C

Table I 1b: Discharge line capacity correction factors for KLEA 407C

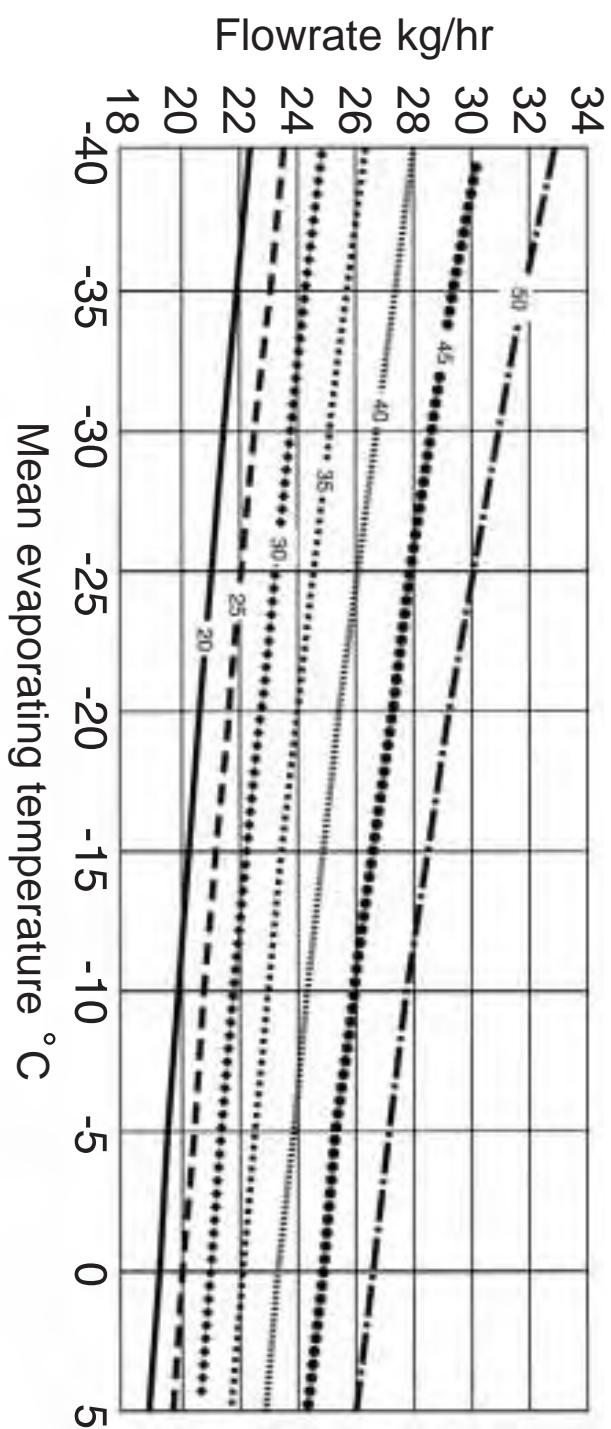
To convert tabulated values to values for true mean condenser temperature multiply by the appropriate factor from this table.

Evap. Temp. °C	Mean Condenser Temperature °C		
	30	40	50
5	0.867	1.000	1.117
0	0.869	1.000	1.114
-5	0.870	1.000	1.111
-10	0.872	1.000	1.108
-15	0.873	1.000	1.104
-20	0.875	1.000	1.100
-25	0.877	1.000	1.097
-30	0.879	1.000	1.093
-35	0.882	1.000	1.089
-40	0.885	1.000	1.086

Note: (i) Condenser temperatures refer to true mean temperature
(ii) Capacities based on saturated vapour leaving evaporator

Refrigerant Flowrate for 1 kW Refrigeration

KLEA 407C



Legend shows liquid temperature at valve inlet °C



KLEA® 407C

mexichem.
FLUOR

**Mexichem UK Limited, The Heath Business and Technical Park,
Runcorn, Cheshire, WA7 4QX
Telephone: +44 (0) 1928 514840
www.mexichemfluor.com**

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